Preparation and Characterization of Mg/TiO₂ for Visible Light Photooxidative-Extractive Deep Desulfurization

(Penyediaan dan Pencirian Mg/TiO₂ untuk Proses Nyahsulfur Fotopengoksidaan-Pengekstrakan di bawah Cahaya Nyata)

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ABSTRACT

A series of Mg/TiO_2 photocatalysts were prepared using aqueous wet impregnation method at different Mg loading followed by calcination at different temperatures for 1 h duration. The photocatalysts were characterized using thermal gravimetry, Fourier-transform infrared spectroscopy, x-ray diffraction, field emission scanning electron microscopy and high-resolution transmission electron microscopy. The photocatalysts were investigated for photooxidative-extractive deep desulfurization of model oil containing dibenzothiophene at room temperature and under visible light irradiation. The model oil containing 100 ppm S was photooxidized followed by extraction using imidazolium-phosphate ionic liquids at room temperature. The best performing photocatalyst was 0.25 wt. % Mg/TiO₂ calcined at 400°C (0.25Mg400), in which 98.4% of dibenzothiophene (3.070 mmol DBT per g photocatalyst) was converted to dibenzothiophene sulfone. The highest extraction efficiency of 97.8% (0.01525 mmol S per mL ionic liquid) was displayed by 1,2-diethylimidazolium diethylphosphate.

Keywords: Desulfurization; Mg/TiO₂; oxidation; photocatalyst; visible light

ABSTRAK

Suatu siri Mg/TiO₂ fotomangkin telah disediakan menggunakan kaedah impregnasi basah akuas dengan komposisi Mg yang berlainan diikuti dengan pengkalsinan selama I jam pada suhu yang berlainan. Pencirian fotomangkin tersebut dijalankan menggunakan termogravimetri, spektroskopi transformasi Fourier inframerah, pembelauan sinar-X, pemancaran medan mikroskopi imbasan elektron dan mikroskopi transmisi elektron beresolusi tinggi. Seterusnya, fotomangkin tersebut dikaji untuk proses nyahsulfur fotopengoksidaan-pengekstrakan daripada model minyak diesel yang mengandungi dibenzotiofen pada suhu bilik dan di bawah sinaran cahaya nyata. Model minyak mengandungi 100 ppm S yang difoto-oksidakan diikuti dengan proses pengekstrakan menggunakan bendalir ionik imidazolium fosfat pada suhu bilik. Fotomangkin 0.25 % bt. Mg/TiO₂ yang dikalsin pada 400°C menunjukkan prestasi yang terbaik dengan 98.4% dibenzotiofen (3.070 mmol DBT per g fotomangkin) ditukar kepada dibenzotiofen sulfon. Tahap tertinggi pengekstrakan yang tercapai adalah 97.8% (0.01525 mmol S per mL bendalir ionik) yang ditunjukkan oleh 1,2-dietilimidazolium dietilfosfat.

Kata kunci: Cahaya nyata; fotomangkin; Mg/TiO,; nyahsulfur; pengoksidaan

INTRODUCTION

In oil and gas industry, the emission of sulfur compounds from petroleum exhaust such as sulfur dioxide, SO_2 , or sulfur trioxide, SO_3 , into the atmosphere is undesirable. These pollutants are detrimental to both environment and human health; causing acid rain, corrosion of buildings and monuments, damaged trees, irritation to eyes, nose, throat and respiratory tract. The Malaysian Government has imposed the regulatory standards for sulfur content in diesel down to 10 ppm, to meet the EURO V standard (EPA 2011). The current industrial method to remove sulfur from diesel is called hydrodesulfurization (HDS). However, this process requires high operating temperature and pressure (approximately 400°C and 100 atm) leading to high operational cost and energy consumption. Furthermore, HDS has its limitation in removing refractory sulfur compounds with high stearic hindrance (Campos-Martin et al. 2010; Jiang et al. 2011a). Therefore it is impossible to reduce the sulfur content in diesel down to less than 10 ppm via HDS.

There are few reported alternatives for sulfur removal that have been researched and investigated. Since the world is moving towards sustainable approach, utilization of the free and abundant sunlight for solar photocatalytic process (An'amt et al. 2014; Khalik et al. 2015) would be attractive. One of the promising processes is photooxidative desulfurization using titania, TiO_2 to remove heterocyclic sulfur compounds such as benzothiophenes (Abdel-Wahab & Gaber 1998; Matsuzawa et al. 2002) and dibenzothiophenes (Abdel-Wahab & Gaber 1998; Tao et al.

2009) from fuel (Abdel-Wahab & Gaber 1998; Matsuzawa et al. 2002) and kerosene (Tao et al. 2009) in the presence of oxidizing agent. TiO_2 , is a semiconductor photocatalyst which shows high activity under ultraviolet rays only. TiO_2 has a band gap of 3.2 eV which confines its photocatalytic activity within the range of UV light (λ <388 nm). Since sunlight consists of less than 5% UV portion, only a small fraction of solar spectrum can be utilized. In order to harvest the visible light portion of the sun, modification by metal doping has been proven to be effective (Afshar et al. 2011; Choi et al. 2010; Feng et al. 2013; Kudo et al. 2007; Linsebigler et al. 1995; Wongpisutpaisan et al. 2013). In principle, the metal dopants can reduce the band gap energy and thus extend the active region of TiO₂ from UV to visible light.

Feng et al. (2013) has reported that modification of TiO₂ with magnesium (Mg) was able to improve its photocatalytic performance under solar radiation. In addition, the photocatalysts also showed impressive recyclability of up to five photocatalytic activity cycles (Feng et al. 2013). The applications of magnesium oxide (MgO) nanomaterials are extremely wide extending from areas in catalysis (Carabineiro et al. 2011; Ganguly et al. 2011; Heidari et al. 2009), to superconductivity (Yuan et al. 1996). This is due to its unique physical and chemical properties. During photocatalyst preparation, the optimum calcination temperature was reported in the range from 400-500°C (Ileperuma et al. 1990; Peng et al. 2004). The presence of magnesium ion, (Mg^{2+}) resulted in the photocatalytic activity being extended to the visible region. The incorporation of Mg²⁺ on TiO₂ did not influence the crystal patterns of TiO₂ particles (Avasarala et al. 2011) as was indicated by XRD data which showed the presence of single anatase phase. Mg/TiO, has been employed in photoreduction process, converting nitrogen into ammonia (Ileperuma et al. 1990) and also in photocatalytic degradation of organophosphate pesticide (monochrotophos) (Avasarala et al. 2011). However, to date it has not been reported by other researchers for deep desulfurization process. In a UV-visible absorption study, the presence of Mg shifted the absorption region to higher wavelength in the visible region (400-550 nm). This observation indicated reduction in band gap. In addition, Avasarala et al. (2011) also proved that the presence of Mg could also reduce the recombination rate of the photogenerated electrons and holes. Combined oxidative-extractive desulfurization (Jiang et al. 2011b; Zhang et al. 2009a, 2009b) has also been reported as one of the desulfurization methods where imidazolium-phosphate ionic liquids displayed good extractive performance (Zaid 2011; Zhang et al. 2009b). Other reported ionic liquid alternatives were quaternary ammonium ionic liquids such as Et, NHCl.FeCl, (Zhao et al. 2011) and choline chlorideglycerol (Zaid et al. 2015) used as extractants.

This paper investigates the performance of Mg/TiO_2 for photooxidation of dibenzothiophene (DBT) in model oil under visible light irradiation. This was followed by extraction of the photooxidized model oil using imidazolium-phosphate ionic liquid. The morphological and structural properties of the Mg/TiO_2 photocatalysts were also investigated.

MATERIALS AND METHODS

PREPARATION OF MG/TIO,

A series of Mg/TiO₂ photocatalysts were prepared using wet impregnation method in aqueous solution. Based on previously reported study on Mg/TiO₂ photocatalyst (Avasarala et al. 2011), it was shown that the optimum performance was achieved employing 1.00 wt. % Mg loading. Therefore, for this study, the amount of Mg loaded onto TiO₂ (Degussa P25) was investigated in the range from 0.10 to 4.00 wt. %. The Mg precursor used for the photocatalyst preparation was magnesium nitrate hexahydrate, Mg(NO₃)₂.6H₂O. All chemicals were used as received.

A premeasured amount of $Mg(NO_2)_2.6H_2O$ was dissolved in distilled water followed by addition of predetermined amount of TiO2. The suspension was continuously stirred for 1 h followed by slow evaporation of the solvent in a water bath at 80°C. Then the material was further dried in an oven at 120°C for 18 h. The dried photocatalyst, termed as uncalcined photocatalyst was ground into fine powder in order to maximize its surface area for calcination. Calcination process was conducted in static air to activate the uncalcined photocatalyst at 300, 400 and 500°C for 1 h duration. Denotation was used to represent the photocatalyst: aMgT where 'a' refers to the Mg loading in wt. % on TiO, and 'T' refers to the calcination temperature in °C. For example, 0.25Mg400 represents 0.25 wt. % Mg loaded onto TiO, and calcined at 400°C.

DESULFURIZATION PROCESS

Deep desulfurization was conducted in two consecutive steps: Photooxidation followed by extraction processes. Sulfur species in the form of dibenzothiophene (DBT) was the model refractory sulfur species used in this work. It was added into dodecane to prepare model oil containing 100 ppm S (equivalent to 3.118 mM DBT) simulating diesel fuel. Photooxidation was conducted in the presence of visible light radiation followed by extraction using ionic liquids. A mixture containing 10 mL model oil and 0.01 g of photocatalyst giving concentration of 1.00 g L⁻¹ Mg/TiO₂ nanoparticles was stirred in the dark for 30 min to ensure homogeneous mixing between DBT and photocatalyst. The mixture was then irradiated with a 500 W halogen lamp. The photoreactor was positioned below the light source (500W halogen lamp (λ >400 nm)) with a distance of 15 cm between the lamp and the top of the model oil. The reaction was carried out for 6 h. Intermittent sampling of the model oil during photoreaction was conducted at different time intervals (every 15 min for the first hour followed by 30 min for

the second hour and every hour after that). The suspended photocatalyst was separated by filtration prior to analysis using GC-SCD (Agilent 7890A gas chromatograph coupled with Agilent 355 sulfur chemiluminescence detector). It was equipped with DB-1 J & W 123-1033 column (30 m \times 320 mm \times 1 mm) referring to the column dimension maintained at 325°C with helium carrier gas flowing at 1.1 mL min⁻¹. The samples were analyzed to determine the amount of S as DBT and also dibenzothiophene sulfone (DBTO₂).

During the photooxidation process, no oxidant was required. The amount of DBT (mmol) being converted to $DBTO_2$ per unit mass of photocatalyst was determined using (1):

$$DBT conversion = \frac{10}{1000} \times \frac{\left(DBT_i - DBT_f\right)}{\text{mass photocat}},$$
 (1)

where DBT_i and DBT_f are the initial and final concentrations of DBT (mM), respectively, in the model oil.

On the other hand, the % DBT conversion was calculated using (2):

$$\% DBT conversion = \frac{\mathbf{s}_i - \mathbf{s}_f}{s_i} \times 100\%, \tag{2}$$

where S_i and S_f are the initial and final concentrations of S (ppm), respectively, in the model oil.

The oxidized model oil (5.0 mL) was further extracted using three different types of ionic liquids (1.0 mL), namely 1,3-dibutyl-imidazolium dibutylphosphate (BBIM[DBP]), 1-butyl-2-ethyl imidazolium diethylphosphate (BEIM[DEP]) and 1,2-diethyl imidazolium diethylphosphate (EEIM[DEP]) to extract the sulfur species (both DBT and DBTO₂). These three ionic liquids were selected based on their outstanding performance reported from previous work on integrated catalytic oxidation-extraction for desulfurization (Zaid 2011). The total amount of S (mmol), both as DBT and DBTO₂ that were extracted per unit volume of ionic liquid was determined using (3):

$$S_{extracted} = \frac{5}{1000} \times (S_o - S_e) \times \frac{1}{\text{volume ionic liquid}}, \quad (3)$$

where S_o and S_e are the total concentrations of sulfur species (mM), as DBT and DBTO₂ in the model oil after photooxidation process and extraction process, respectively.

In order to determine the % $S_{removal}$, (4) was used:

$$\% S_{removal} = \frac{s_o - s_e}{s_o} \times 100\%,$$
 (4)

where S_o and S_e are the total concentrations of sulfur species (ppm) as DBT and DBTO₂ in the model oil after photooxidation process and extraction process, respectively.

CHARACTERIZATION OF PHOTOCATALYST

Selected photocatalysts were characterized using thermal gravimetric analysis (TGA), Fourier-transform infrared spectroscopy (FTIR), x-ray diffraction (XRD), field emission scanning electron microscopy (FESEM) and high-resolution transmission electron microscopy (HRTEM). TGA was conducted using Perkin Elmer Thermal Analyzer (Pyris V3.81) to estimate suitable calcination temperatures for activating the raw photocatalyst. In FTIR, the IR spectrum was collected by scanning the sample from 4000 to 400 cm⁻¹ in the transmission mode using Perkin Elmer spectrophotometer (Spectrum One). The resulting FTIR spectra were used to analyse and identify the functional groups present in the photocatalyst. The effect of incorporating Mg onto the crystal structure of TiO, was analyzed using powder XRD (Bruker D8 Advance) conducted with CuKa radiation (40 kV, 40 mA) at 20 angles from 2° to 80° and a scan speed of 4° min⁻¹. This technique is used to identify the type of TiO, phases and Mg-species present. The morphology of the Mg/TiO₂ photocatalysts was determined using FESEM (Zeiss Supra 35VP). The samples were coated with a layer of platinumpalladium prior to scanning at 100 kX magnification. HRTEM was performed using Zeiss Libra 200 microscopy technique whereby a beam of electrons was transmitted through an ultra-thin sample. The image formed from the interaction of the electrons transmitted through the sample is magnified and focused onto an imaging device.

RESULTS AND DISCUSSION

PRETREATMENT OF PHOTOCATALYST

The thermograms for the raw and calcined Mg/TiO_2 photocatalysts are displayed in Figure 1. The raw materials were thermally stable. Slight decomposition was observed (less than 10%) when the temperature was increased to 800°C. The raw photocatalyst (0.25 Mg uncalcined) decomposed slightly more than the calcined samples



FIGURE 1. Thermogram of uncalcined and calcined photocatalysts with different Mg loading

which may be related to the presence of hydrates (50-200°C). Higher degradation temperature displayed on the thermograms may indicate the decomposition of $Mg(NO_3)_2$ as proposed in (2) (Clark 2005).

$$2Mg(NO_3)_2(s) \rightarrow 2 MgO(s) + 4NO_2(g) + O_2(g). \quad (2)$$

DESULFURIZATION PROCESS

Photooxidation which is the first step in deep desulfurization process was conducted using Mg/ TiO₂ photocatalysts for a duration of 6 h under visible light irradiation. No oxidant was added. The effect of calcination temperature and Mg loading on DBT conversion were investigated and the results are shown in Figure 2. Equations (2) and (3) were used to calculate DBT conversion. Calcination temperature at 300°C was not producing active photocatalysts where the performance was less than 5% (0.130 mmol DBT per g photocatalyst). After calcination at 400°C, photocatalyst with 0.5 wt. % Mg loading (0.5 Mg400) showed the best performance of 45.7% DBT conversion to DTBO, (1.426 mmol DBT per g photocatalyst). Therefore, lower Mg loading photocatalysts were further investigated (0.10-0.25 wt. %) to determine its effect on activity.



FIGURE 2. Effect of Mg loading and calcination temperature on DBT conversion to DBTO₂

Figure 3(a) shows the improved performance of Mg/ TiO₂ photocatalysts with lower Mg loading calcined at 400°C. The best performing photocatalyst was that with 0.25 wt. % Mg loading (0.25 Mg400) giving 98.4% DBT conversion (3.070 mmol DBT per g phoocatalyst) after 5 h reaction. Then, the effect of calcination temperature (300 and 500°C) on the performance of 0.25 wt. % Mg/ TiO₂ photocatalysts was further investigated. Based on Figure 3(b), although the photocatalyst calcined at 500°C displayed better performance (3.073 mmol DBT per g photocatalyst), it could only outperform 0.25 Mg400 by 0.2%, thus, 400°C is still the preferred optimum calcination temperature since it is less energy intensive.

Photolysis of DBT was negligible (0.02%). The oxidized model oil (containing both DBT and DBTO₂) was further extracted by using three imidazolium-phosphate type ionic liquids, (BBIM[DBP], (BEIM[DEP]) and (EEIM[DEP]). The extraction efficiencies were determined using (3) and (4). Figure 4 shows the extraction efficiency of the three imidazolium-phosphate-based ionic liquids. The performance of all three ionic liquids were comparable with the extraction efficiencies of BBIM[DBP], BEIM[DEP] and EEIM[DEP] at 97.2% (0.01515 mmol S per mL ionic liquid), 97.7% (0.01523 mmol S per mL ionic liquid) and 97.8% (0.01525 mmol S per mL ionic liquid), respectively. Previous work on the oxidative-extractive desulfurization from 1000 ppm DBT (with addition of H_2O_2 (Zaid 2011) showed that the sulfur removal was in the range from 78.2-85.2% following the sequence of BBIMDBP > EEIMDEP > BEIMDEP. To date, no other work has been reported on similar Mg/TiO₂ photocatalyst for deep desulfurization process. Photooxidative-extractive desulfurization process under UV (Zhao et al. 2011) and visible light irradiation (Zaid et al. 2015) using TiO₂-based photocatalyst and quaternary ammonium ionic liquids have been reported with comparative sulfur removal efficiency of more than 98% and 97.1%, respectively.



FIGURE 3. Effect of (a) Mg loading and (b) calcination temperature on DBT conversion



FIGURE 4. Extraction efficiency of total sulfur species using different ionic liquids

CHARACTERIZATION RESULTS

FTIR

Figure 5(a) compares the FTIR spectra of the uncalcined and calcined photacatalysts showing the presence of nitrate functional group at wavenumber 1384 cm⁻¹ (Nakagawa & Walter 1969) on the raw photocatalyst. There was no indication of the presence of nitrate group in the calcined samples indicating that the nitrate group was completely removed during calcination process (Clark 2005). This is in agreement with the results obtained from TGA. Based on Figure 5(a) and 5(b), all photocatalysts displayed the absorption bands corresponding to O–H stretching and bending around 3400 and 1600 cm⁻¹, respectively. However, the % transmittance of the characteristic peaks before calcination was higher compared to that after calcination. This indicates that most of the hydrates were removed during calcination, in agreement with the TGA results. An absorption band between 400 and 900 cm⁻¹ was attributed to Ti–O stretching vibrations (Wang & Zhou 2010).



FIGURE 5. FTIR spectra for (a) uncalcined and calcined Mg/TiO₂ photocatalysts and (b) Mg/TiO, photocatalysts



FIGURE 6. XRD pattern of 0.24 Mg400

XRD

The XRD pattern of 0.25 Mg400 displayed in Figure 6 shows the characteristic peaks for TiO₂ dominated by the anatase phase (A) $(2\theta = 25.3^{\circ}, 33.8^{\circ}, 47.8^{\circ}, 53.8^{\circ})$ and a small amount of rutile phase (R) $(2\theta = 27.4^{\circ})$.

No peaks corresponding to Mg-species were detected indicating high Mg dispersion on TiO_2 . Similar results were also observed by Avasarala et al. (2011). The XRD patterns for the other photocatalysts with different Mg loadings and calcined at different temperatures were similar to that represented in Figure 6.

FESEM

Figure 7(a)-7(d) displays the FESEM images for Mg/ TiO₂ photocatalysts with different Mg loading calcined at 400°C for 1 h duration. The average particle size and particle size distribution of the photocatalysts are shown in Table 1. Figure 7(a)-7(c) shows irregular sphericalshaped particles with size ranging from 17-62 nm. The photocatalysts maintained their average size within 26-31 nm, comparable to as reported the literature (Avasarala et al. 2011; Hwang et al. 2009). As the Mg loading increased, the particle size also increased in addition to the presence of cubical-shaped structural materials (indicated by white circle in Figure 7(d)). This may represent the presence of separate Mg particles (Su et al. 2011). Agglomeration and sintering of the nanoparticles were also observed with the increase in size distribution.

HRTEM

Figure 8(a)-8(d) displays the HRTEM images and lattice fringes of the Mg/TiO₂ photocatalysts with different Mg loading and calcined at 400°C. Two different morphologies were observed; irregular spherical-shaped and also cubicalshaped particles (indicated by white circle in Figure 8(c)) which may represent TiO₂ and Mg-species, respectively (Su et al. 2011). Two different length of lattice fringes were also identified from which were tabulated in Table 2. The shorter and more consistent d-spacing of 0.332-0.361 nm was assigned to anatase TiO₂ (101) (Lu et al. 2008; Parra et al. 2008; Zhang et al. 2011). No surface lattice distortion on TiO, was observed even when incorporated with higher Mg loading (Zhang et al. 2011). The longer d-spacing ranging from 0.753-1.230 nm may be related to Mg-species. The reported lattice fringes for Mg-species were 0.21 nm for MgO (200) (Ganguly et al. 2011; Kim et al. 2006; Su et al. 2011); 1.64 and 1.07 nm for lamellar Mg(OH), (200) and (300) (Ranjit & Klabunde 2005); 0.72 nm for mixture of



FIGURE 7. FESEM images for (a) 0.10 Mg, (b) 0.25 Mg, (c) 0.50 Mg and (d) 1.00 Mg photocatalysts

Mg loading (%)	Average particle size (nm)	Particle size range (nm)
0.10	26	17-57
0.25	31	20-62
0.50	31	23-45
1.00	35	22-62

TABLE 1. Particle size distribution and average size of Mg/TiO, photocatalyst

MgO and $Mg(OH)_2$ (Mc Kelvy et al. 2001) and 0.89-0.96 nm for lamellar Mg-oxyhydroxide intermediates (Mc Kelvy et al. 2001).

Based on the d-spacings indicated in Table 2, coexistence of MgO and $Mg(OH)_2$ was observed at low Mg loading while the presence of lamellar Mg-oxyhydroxide intermediate was observed on 0.25 Mg400. At higher Mg loading, lamellar Mg(OH)₂ was present. The best performing photocatalyst for deep desulfurization was 0.25 Mg (Zaid 2011) indicating that the active species required for the process was lamellar Mg-oxyhydroxide intermediates.

CONCLUSION

 Mg/TiO_2 was successfully synthesized using aqueous wet impregnation method. 0.25 Mg400 has successfully



FIGURE 8. HRTEM images for (a) 0.10 Mg, (b) 0.25 Mg, (c) 0.50 Mg and (d) 1.00 Mg photocatalysts

Malanding (%)	d specing of TiO (nm)	Mg-Species	
Nig loading (%)	d-spacing of 110_2 (iiii)	d-spacing (nm)	Type of Mg-Species
0.10	0.361	0.753	$MgO + Mg(OH)_2$ mixture
0.25	0.358	0.881	Mg-oxyhydroxide lamellar
0.50	0.359	1.073	Mg(OH) ₂
1.00	0.332	1.113	Mg(OH) ₂

TABLE 2. HRTEM d-spacings of Mg/TiO, photocatalyst

photooxidized 98.4% of DBT (3.070 mmol DBT per g photooxidized 98.4% of DBT (3.070 mmol DBT per g photocatalyst) into DBTO₂. The sulfur removal observed after subsequent extraction with 1,2-diethyl imidazolium diethylphosphate (EEIM[DEP]) ionic liquid gave the highest performance of 97.8 % (0.01525 mmol S per mL ionic liquid). Mg/TiO₂ exist as irregular spherical-shaped particles. As the Mg loading increased, cubical shaped structure materials could be observed. The average particle size ranged from 26-36 nm. Incorporation of Mg on TiO₂ did not lead to any lattice distortion. At low Mg loading, the presence of MgO + Mg(OH)₂ mixture was detected while at higher Mg loading, the presence of lamellar Mg-oxyhydroxide intermediates were the active species for high photooxidative performance.

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